

MECHANIK der Kontinua - Klausur 09 - LösungenTEIL A

1

$$(a) \frac{d\vec{A}}{dt} = \frac{\partial \vec{A}}{\partial t} + (\vec{v} \cdot \nabla) \vec{A}$$

$$(b) \frac{\partial \rho}{\partial t} + \nabla \cdot (\rho \vec{u}) = 0 \quad \xrightarrow{\nabla \cdot} \quad \text{for incompressible flow} \quad \nabla \cdot \vec{u} = 0$$

$$(c) \rho \frac{dv_i}{dt} = \rho F_i - \nabla_i p + \eta \nabla_j \nabla_j v_i + (\eta + \eta') \nabla_i \nabla_j v_j$$

$$\text{for incompressible flow} \rightarrow \rho \frac{dv_i}{dt} = \rho F_i - \nabla_i p + \eta \nabla_j \nabla_j v_i \quad \text{Navier equation.}$$

2

(i) For 2-D, incompressible, irrotational flows

$$(ii) w(z) = \phi(z) + i\psi(z)$$

$$(iii) v_x = u = \frac{\partial \phi}{\partial x} = \frac{\partial \psi}{\partial y} \quad ; \quad v_y = v = \frac{\partial \phi}{\partial y} = -\frac{\partial \psi}{\partial x}$$

3

$$(i) Re = \frac{vL}{\nu} = \frac{vLe}{\eta} \quad \left(Re = \frac{\text{viscous force}}{\text{inertia force}} \right)$$

v = velocity
 L = width
 ν = viscosity (kinematic)
 ρ = density
 η = dynamic viscosity

(ii) 2 flows are similar when their Reynold's numbers are the same: $Re_1 = Re_2$

$$(iii) Re = \frac{uL}{\nu} = \frac{v_{\text{char}} \rho}{\eta} = 2000 \quad (\text{laminar flow})$$

4

$$\sigma_{ij} = 2S_{ij}\epsilon_{ij} + 2\lambda\epsilon_{ij} \quad ; \quad S_{ij} \hat{=} \text{Lame constants}$$

$$\sigma_{ij} \hat{=} \text{stress tensor}$$

$$\epsilon_{ij} \hat{=} \text{strain tensor}$$

$$\epsilon_{ij} = \frac{1}{2} \left(\frac{\partial s_j}{\partial i} + \frac{\partial s_i}{\partial j} \right)$$

velocity potential \downarrow
 $\Phi + \frac{v^2}{2} + U + \Pi = \text{const}$
 velocity \swarrow
 potential energy \swarrow
 pressure gradient \swarrow

$\Phi \hat{=}$ velocity potential
 $v \hat{=}$ velocity
 $U \hat{=}$ gradient of forces
 $\Pi \hat{=}$ gradient of pressure

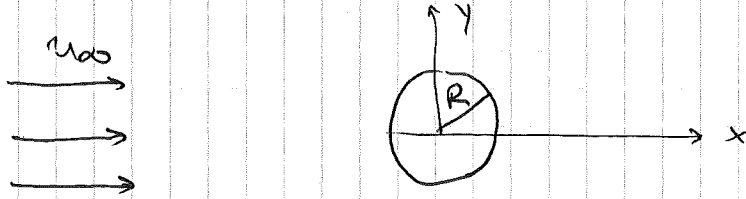
valid along a streamline

for rotational flows

[In general Bernoulli's principle is equivalent to the principle of energy conservation (in a steady flow, the sum of all forms of mechanical energy in a fluid a streamline is the same at all points on that streamline)]

TEIL B

G



$$W(z) = u_{\infty} \left(z + \frac{R^2}{z} \right) - i \frac{\Gamma}{2\pi} \ln z$$

(a) $z = r e^{i\vartheta}$

$$\Rightarrow W(z) = u_{\infty} \left(r e^{i\vartheta} + \frac{R^2}{r e^{i\vartheta}} \right) - i \frac{\Gamma}{2\pi} \ln(r e^{i\vartheta})$$

$$= u_{\infty} \left(r e^{i\vartheta} + \frac{R^2}{r} e^{-i\vartheta} \right) - i \frac{\Gamma}{2\pi} [\ln r + i\vartheta]$$

$$= u_{\infty} \left(r(\cos\vartheta + i\sin\vartheta) + \frac{R^2}{r} (\cos\vartheta - i\sin\vartheta) \right) - i \frac{\Gamma}{2\pi} (\ln r + i\vartheta)$$

$$= \left[u_{\infty} r \cos\vartheta \left(1 + \frac{R^2}{r^2} \right) + \frac{\Gamma}{2\pi} \vartheta \right] + i \left[u_{\infty} r \sin\vartheta \left(1 - \frac{R^2}{r^2} \right) - \frac{\Gamma}{2\pi} \ln r \right]$$

$$= \Phi + i\Psi$$

$$\Rightarrow \int \Phi(r, \vartheta) = u_{\infty} r \cos\vartheta \left(1 + \frac{R^2}{r^2} \right) + \frac{\Gamma}{2\pi} \vartheta$$

$$\int \Psi(r, \vartheta) = u_{\infty} r \sin\vartheta \left(1 - \frac{R^2}{r^2} \right) - \frac{\Gamma}{2\pi} \ln r$$

(b) $u_r = \frac{1}{r} \frac{\partial \Psi}{\partial \vartheta} = u_{\infty} \left[1 - \frac{R^2}{r^2} \right] \cos\vartheta$

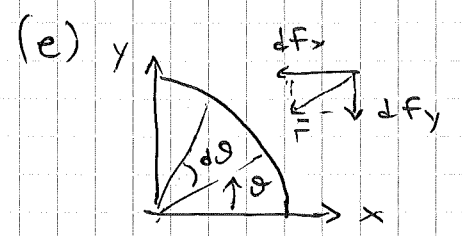
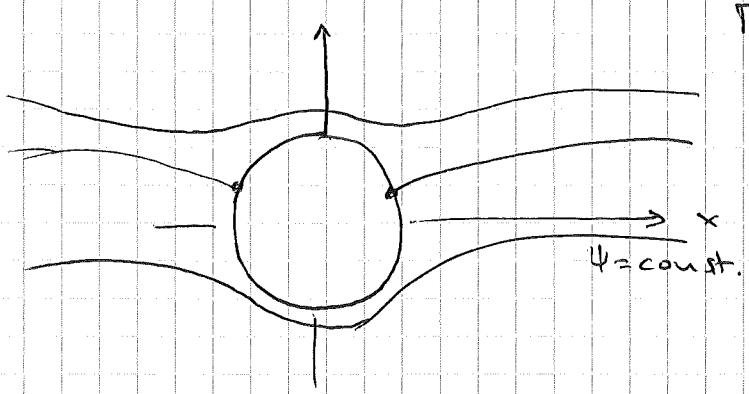
$$u_{\vartheta} = \frac{\partial \Phi}{\partial r} = u_{\infty} \left[1 + \frac{R^2}{r^2} \right] \sin\vartheta + \frac{\Gamma}{2\pi r}$$

(c) $r=R : u_\theta = \frac{\Gamma}{2\pi R} \equiv u_\infty \Rightarrow \Gamma = 2\pi u_\infty R \quad \textcircled{+}$

circulation $\equiv \oint \vec{u} \cdot d\vec{\ell} = \oint (u_r \hat{r} + u_\theta \hat{\theta}) \cdot R d\theta \hat{\theta} =$
 $= \oint u_\theta R d\theta = R \int_0^{2\pi} \left[-u_\infty \left(1 + \frac{R^2}{r^2}\right) \sin\theta + \frac{\Gamma}{2\pi R} \right] d\theta$
 $= R \frac{\Gamma}{2\pi R} 2\pi \equiv \Gamma$

(d) stagnation points: $u=0$ at $r=R : u_r(r=R)=0$
 $u_\theta(r=R) = -2u_\infty \sin\theta + \frac{\Gamma}{2\pi R}$

$\rightarrow u_\theta(r=R)=0 \Rightarrow \sin\theta_{sp} = \frac{\Gamma}{4\pi R u_\infty} \left\{ \begin{array}{l} \rightarrow \sin\theta_{sp} = \frac{1}{2} \Rightarrow \\ \Gamma = 2\pi u_\infty R \end{array} \right.$
 $\theta_{sp} = \frac{\pi}{6}, \frac{5\pi}{6}$



$dF_x = -p L R \cos\theta d\theta$
 $dF_y = -p L R \sin\theta d\theta$
 but $p = p_\infty + c_p \frac{\rho}{2} u_\infty^2$

at $r=R : c_p = 1 - \left[\frac{u_t}{u_\infty} - 2\sin\theta \right]^2$ $u_t = u_{\text{tangential}}$

$\Rightarrow F_x = -LR \int_0^{2\pi} \left\{ \frac{\rho}{2} u_\infty^2 \left[1 - \left(\frac{u_t}{u_\infty} - 2\sin\theta \right)^2 \right] + p_\infty \right\} \cos\theta d\theta = 0$

$F_y = -LR \int_0^{2\pi} \left\{ \frac{\rho}{2} u_\infty^2 \left[1 - \left(\frac{u_t}{u_\infty} - 2\sin\theta \right)^2 \right] + p_\infty \right\} \sin\theta d\theta =$
 $= -2\pi \rho L R u_\infty = -\rho u_\infty \Gamma L$

or from Blasius formula:

$F_x - i F_y = \frac{i\rho}{2} \oint_c \left(\frac{dw}{dz} \right)^2 dz$

$$\frac{dw}{dz} = u_{\infty} \left(1 - \frac{R^2}{z^2} \right) - i \frac{\Gamma}{2\pi z}$$

$$\Rightarrow F_x - i F_y = \frac{1}{2} i \rho \oint_C \left[u_{\infty} \left(1 - \frac{R^2}{z^2} \right) - i \frac{\Gamma}{2\pi z} \right]^2 dz =$$

$$= \frac{1}{2} i \rho \cdot 2\pi i \left(- \frac{i u_{\infty} \Gamma}{\pi} \right) = \rho u_{\infty} \Gamma$$

$$\Rightarrow \begin{cases} F_x = 0 \\ F_y = \rho u_{\infty} \Gamma \end{cases} \quad \left(\begin{array}{l} \text{in the integral only } \frac{1}{z} \text{ term} \\ \text{contributes with its residual} \\ \text{Res}(z=0) \end{array} \right)$$

7 (e) dynamic boundary condition at wall: $u = v_x(y=0) = 0$
and $\lim_{y \rightarrow \infty} v_x(y) = u_{\infty}$ or $v_x(y=\delta) = u_{\infty}$

at wall $v_y(y=0) = -v_a$

(b) $\rho = \text{const.} \rightarrow \frac{D\rho}{Dt} = 0 \rightarrow$ continuity eq.: $\frac{\partial v_x}{\partial x} + \frac{\partial v_y}{\partial y} + \frac{\partial v_z}{\partial z} = 0$

planar flow: $\frac{\partial}{\partial z} = 0$; also $\frac{\partial v_x}{\partial x} = 0 \Rightarrow \frac{\partial v_y}{\partial y} = 0$

$$\Rightarrow \left. \begin{array}{l} v_y = v_y(x) = \text{const} \\ v_y(y=0) = -v_a \end{array} \right\} \rightarrow v_y = -v_a = \text{const. throughout the flow}$$

(c) with $v_y = -v_a$, $\frac{\partial v_x}{\partial x} = 0$, $\frac{\partial v_z}{\partial z} = 0$, constant pressure, no body forces, steady flow \Rightarrow

$$-\rho v_a \frac{\partial v_x}{\partial y} = \eta \frac{\partial^2 v_x}{\partial y^2} \rightarrow -v_a \frac{dv_x}{dy} = \nu \frac{d^2 v_x}{dy^2} \Rightarrow$$

(solution) $\Rightarrow v_x(y) = C_1 + C_2 e^{-\frac{v_a}{\nu} y}$
boundary conditions $\rightarrow C_1 = -C_2 = u_{\infty}$
 $\Rightarrow v_x(y) = u_{\infty} \left(1 - e^{-\frac{v_a}{\nu} y} \right)$
viscosity ν

(d) Newtonian fluid (Cauchy - Poisson law):

$$\sigma_{ij} = -p \delta_{ij} + \lambda^* \varepsilon_{kk} \delta_{ij} + 2\eta \varepsilon_{ij}$$

only non-zero component on the plate surface

$$\sigma_{xy} \Big|_{y=0} = 2\eta \varepsilon_{xy} \Big|_{y=0} = \eta \frac{\partial v_x}{\partial y} \Big|_{y=0}$$

$$\text{from (c)} : \frac{\partial v_x}{\partial y} \Big|_{y=0} = u_{\infty} \frac{v_{\infty}}{r} e^{-\frac{v_{\infty} y}{r}} \Big|_{y=0} = u_{\infty} \frac{v_{\infty}}{r}$$

$$\Rightarrow \sigma_{xy} \Big|_{y=0} = \rho u_{\infty} v_{\infty}$$

8

$$(a) \text{ Bernoulli eq: } p_1 + \frac{\rho}{2} v_1^2 = p_2 + \frac{\rho}{2} v_2^2$$

$$\text{continuity eq: } v_1 A_1 = v_2 A_2 = v_3 A_3$$

$$v_2 = \sqrt{\frac{2 \Delta p}{\rho \left(1 - \left(\frac{A_2}{A_1}\right)^2\right)}} = 12 \text{ m/s}$$

$$\Rightarrow v_1 = 4 \text{ m/s} ; v_3 = 6 \text{ m/s}$$

$$(b) \text{ Bernoulli eq: } p_2 + \frac{\rho}{2} v_2^2 = p_3 + \frac{\rho}{2} v_3^2$$

$$p_3 = p_2 = 10^5 \text{ N/m}^2 \text{ (outflow to the surrounding)}$$

$$\Rightarrow p_2 = 0,46 \cdot 10^5 \text{ N/m}^2$$

$$\text{similar for } p_1 \rightarrow p_1 = 1,1 \cdot 10^5 \text{ N/m}^2$$

$$\text{Bernoulli eq: } p + \rho g h = p_2 + \frac{\rho}{2} v_2^2$$

$$\Rightarrow p = 1,08 \cdot 10^5 \text{ N/m}^2$$

9 cylindrical symmetry \rightarrow Navier Stokes: $\frac{d}{dr} \left[\frac{1}{r} \frac{d(r u_\phi)}{dr} \right] = 0$
(NS)

(from ϕ component of NS eq in cylindrical coordinates with $u_r, u_z = 0$)

$$\Rightarrow u_\phi(r) = C_1 r + \frac{C_2}{r}$$

boundary conditions $\left\{ \begin{array}{l} u_\phi(R_0) = \omega_0 R_0 = C_1 R_0 + \frac{C_2}{R_0} \\ u_\phi(R_1) = \omega_1 R_1 = C_1 R_1 + \frac{C_2}{R_1} \end{array} \right. \Rightarrow$

$$\Rightarrow C_1 = \frac{\Omega_0 R_0^2 - \Omega_1 R_1^2}{R_0^2 - R_1^2}$$

$$C_2 = \frac{(\Omega_1 - \Omega_0) R_1^2 R_0^2}{R_0^2 - R_1^2}$$

from r -component of NS in cylindrical coordinates:

$$\frac{dp}{dr} = \frac{\rho}{r} u_\phi^2 = \frac{\rho}{r} \left(C_1 r + \frac{C_2}{r} \right)^2$$

$$\Rightarrow p(r) = \frac{\rho}{2} \left(\frac{\Omega_0 R_0^2 - \Omega_1 R_1^2}{R_0^2 - R_1^2} \right)^2 r^2 + 2\rho \frac{\Omega_0 R_0^2 - \Omega_1 R_1^2}{R_0^2 - R_1^2} \frac{(\Omega_1 - \Omega_0) R_1^2 R_0^2}{R_0^2 - R_1^2} \frac{1}{r} + \text{const.}$$

(in incompressible flow without pressure boundary conditions, the pressure can be determined only up to a constant)

$$\begin{aligned} \vec{\nabla} \times \vec{u} &= \frac{1}{r} \left(\frac{\partial}{\partial r} (r u_\phi) - \frac{\partial u_r}{\partial \phi} \right) \hat{e}_z = \frac{1}{r} \frac{d}{dr} (C_1 r^2 + C_2) \hat{e}_z \\ &= 2C_1 \hat{e}_z \end{aligned}$$

for irrotational flow: $\vec{\nabla} \times \vec{u} = 0 \Rightarrow C_1 = 0 \Rightarrow$
 $\Omega_0 R_0^2 = \Omega_1 R_1^2 \Rightarrow \frac{\Omega_0}{\Omega_1} = \left(\frac{R_1}{R_0} \right)^2$ viscous potential flow

10

$$\vec{s} = 5x\hat{e}_x + (y+2z)\hat{e}_y + (2y+z)\hat{e}_z$$

$$\epsilon_{ij} = \frac{1}{2} \left(\frac{\partial s_j}{\partial x_i} + \frac{\partial s_i}{\partial x_j} \right)$$

$$\omega_{ij} = \frac{1}{2} \left(\frac{\partial s_j}{\partial x_i} - \frac{\partial s_i}{\partial x_j} \right)$$

$$\sigma_{ij} = \lambda \epsilon_{ij} + \mu \omega_{ij}$$

$$\Rightarrow \epsilon_{ij} = \begin{pmatrix} 5 & 0 & 0 \\ 0 & 1 & 2 \\ 0 & 2 & 1 \end{pmatrix}, \omega_{ij} = \begin{pmatrix} 0 & 0 & 0 \\ 0 & 0 & 0 \\ 0 & 0 & 0 \end{pmatrix}$$

$$\sigma_{ij} = \begin{pmatrix} 7z+10\mu & 0 & 0 \\ 0 & 7z+2\mu & 4\mu \\ 0 & 4\mu & 7z+2\mu \end{pmatrix}$$

$$\det |\sigma_{ij} - \lambda \delta_{ij}| = 0 \Rightarrow \begin{vmatrix} 5-\lambda & 0 & 0 \\ 0 & 1-\lambda & 2 \\ 0 & 2 & 1-\lambda \end{vmatrix} = 0 \rightarrow$$

$$(5-\lambda) [(1-\lambda)^2 - 4] = 0 \Rightarrow \lambda_1 = 5, \lambda_2 = 3, \lambda_3 = -1$$

$$\epsilon_{ij} \begin{pmatrix} x \\ y \\ z \end{pmatrix} = \lambda \begin{pmatrix} x \\ y \\ z \end{pmatrix}$$

$$\lambda_1 = 5: \begin{pmatrix} 5 & 0 & 0 \\ 0 & 1 & 2 \\ 0 & 2 & 1 \end{pmatrix} \begin{pmatrix} x \\ y \\ z \end{pmatrix} = 5 \begin{pmatrix} x \\ y \\ z \end{pmatrix} \rightarrow (x, y, z)_1 = (0, 1, 2)$$

$$\lambda_2 = 3 \rightarrow (x, y, z)_2 = (0, 1, 1)$$

$$\lambda_3 = -1 \rightarrow (x, y, z)_3 = (0, 1, -1)$$